

Tertiary Wastewater Treatment & Advanced Gasification

CALWMC

9th June, 2015

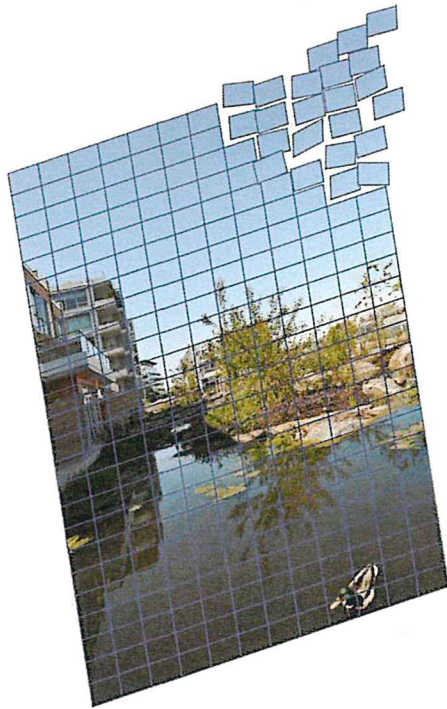
Graeme Bethell
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Matt Hart

Introduction : Integrated Wastewater Treatment Solutions

- Wastewater Treatment
 - ◆ Fixed bed biofilm technology
 - ◆ Norwegian
 - ◆ Fabricated in US, Canada, Norway
- Biosolids Treatment
 - ◆ Advanced gasification
 - ◆ US, Austria & Italy
 - ◆ Fabricated in Sidney BC & the US
- Integrated Resource Management
 - ◆ Optimizes efficiencies & resource recovery
 - ◆ Combined business case





Biowater Technology

Continuous Flow Intermittent Cleaning

Liquid Waste Treatment

Proposed System

Primary Treatment

Salsnes Filter



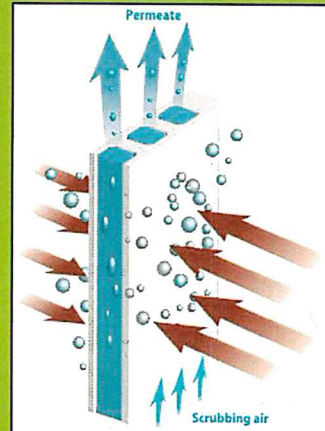
Secondary Treatment

CFIC® System



Tertiary Treatment

Ultrafiltration Membranes



Sludge Management

Advanced Gasifier

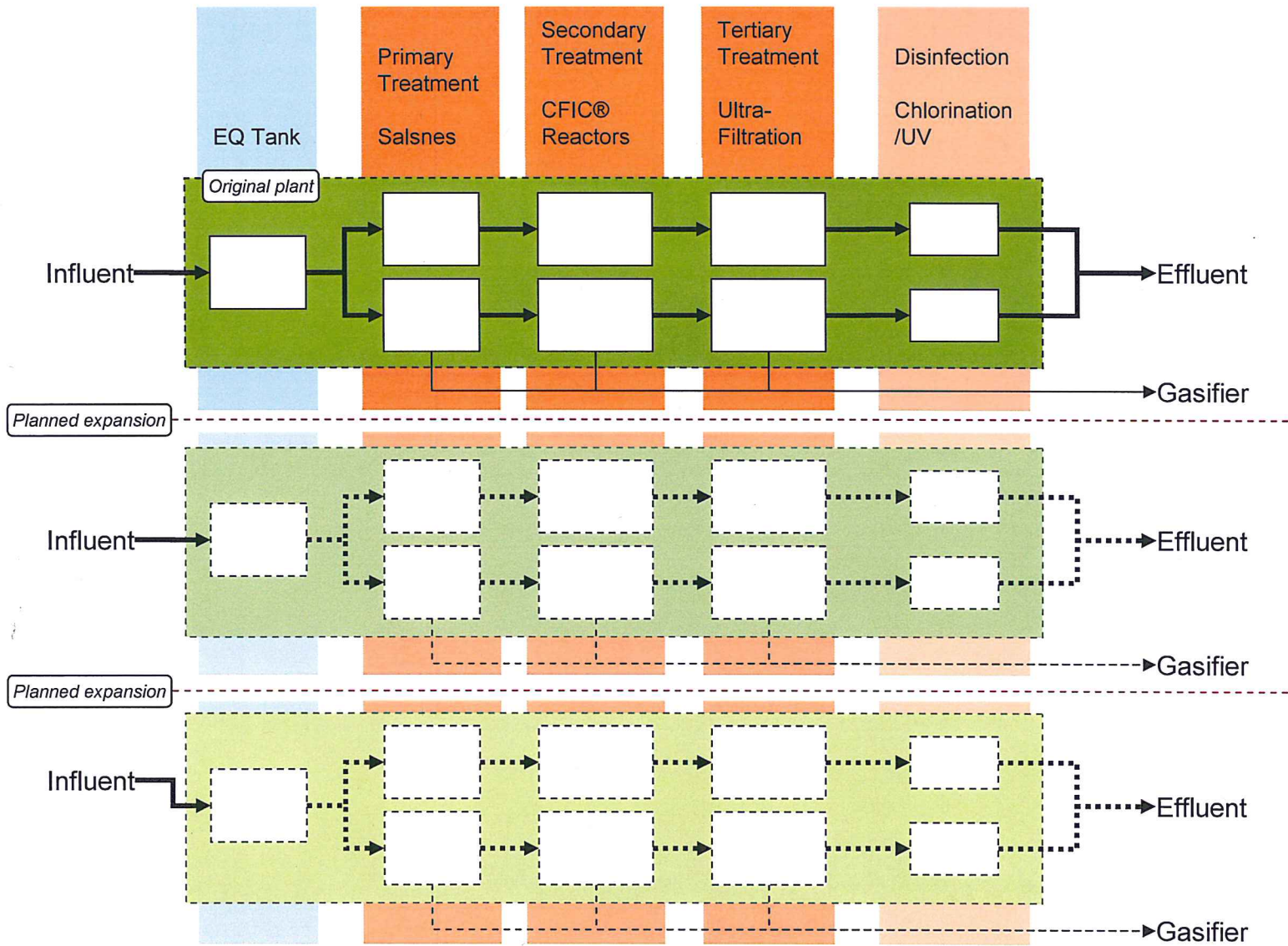


Process

- Grit and trash removed
- Primary treatment is screened to separate sludge and water
 - ◆ Designed for 4x avg. dry weather flow
- CFIC[®] biofilm carriers provide secondary treatment to remove organic material
 - ◆ Designed for 2x avg. dry weather flow
 - ◆ Removes nitrogen
 - ◆ Exceeds treatment standards
- Tertiary treatment using ultrafiltration
- Disinfection
- Sludge → thickened → gasifier



Simple Modular Expansion



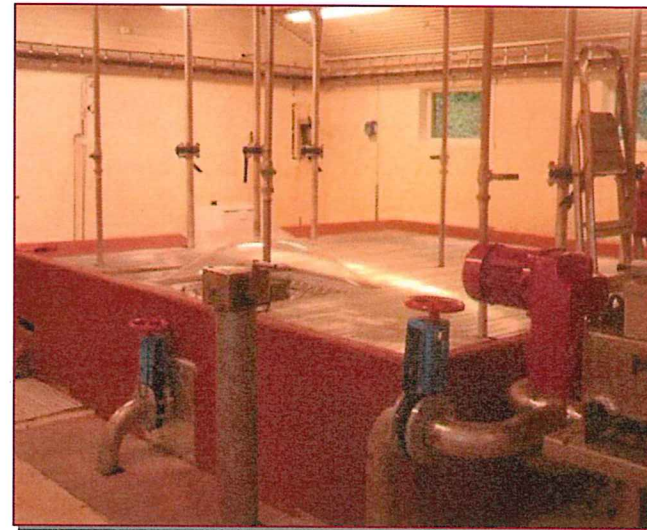
Project	Client	Nature	New/upgrade	Year/status	Country	Type	ML/day	BOD mg/L	Media Type/ Quantity m ³
1 Vike RA	Hof Kommune	Municipal	Upgrade	2009	Norway	A	1.68 MLd	182	BWT-X/30
2 Kimberly Clark	Haztec	Pulp, Paper	Upgrade	2009	Brazil	B	4.80 MLd	600	BWT35/10
3 Standard Process	Environmental Health	Food & Bev	Upgrade	2009	USA	D	0.77 MLd	1,500	BWT-X/35
4 Trysil RA	Municipality of Trysil	Municipal	New	2010	Norway	E	10.73 MLd	225	BWT-X/252
5 Vigor, Sao Paulo	Acqua Engenharia	Dairy	Upgrade	2010	Brazil	B	1.20 MLd	1,800	BWT35/246
6 Harestua RA	Municipality of Lunnar	Municipal	Upgrade	2011	Norway	F	1.92 MLd	180	BWT-X/58
7 Elverom RA	Norde Land Municipality	Municipal	Upgrade	2011	Norway	B	0.24 MLd	150	BWT-X/8
8 Medite	Evergreen Engineering	Pulp, Paper	Upgrade	2011	Ireland	B	1.20 MLd	2,000	BWT-X/143
9 Pachuca STP	Iberaltec	Municipal	Upgrade	2011	Mexico	D	8.64 MLd	350	BWT15/390
10 Sintek	Eco Digital	Electronics	Upgrade	2011	Taiwan	D	1.49 MLd	400	BWT35/380
11 Nordfjord Kjott	Nordfjord Kjott	Food & Bev	Upgrade	2011	Norway	C	0.58 MLd	1,650	BWT-X/57
12 Aaregau WWTP	JS Umwelttechnik	Municipal	Upgrade	2012	Switzerland	D	2.02 MLd	194	BWT15/84
13 Roros RA	Roros Kommune	Municipal	Upgrade	2012	Norway	A	4.80 MLd	186	BWTX/115
14 Flums	JS Umwelttechnik	Municipal	Upgrade	2012	Switzerland	D	3.60 MLd	200	BWT15/150
15 Wetico	Weitco	Industrial	New	2012	Saudi Arabia	A	2.02 MLd	250	BWTX/232
16 Kan PaK	Kan Pak	Food & Bev	New	2012	USA	A	0.98 MLd	2880	BWTX/300
17 Schoftland	JS Umwelttechnik	Municipal	Upgrade	2012	Switzerland	D	4.01 MLd	168	BWT15/205
18 Bloomingdale	Fleis & Vanderbrink Eng.	Municipal	Upgrade	2013	USA	A	0.46 MLd	575	BWTX/129
19 Barlidalen	Barlidalen Municipality	Municipal	Upgrade	2012	Norway	A	20.40 MLd	120	BWTX
20 Saignelegier	JS Umwelttechnik	Municipal	Upgrade	2012	Switzerland	A	1.44 MLd	233	BWT15/193
21 Langmatt	JS Umwelttechnik	Municipal	Upgrade	2012	Switzerland	D	28.70 MLd	91	BWT15/496
22 Teck Coal	H ₂ Flow	Mining	New	Under Constrn	Canada	A	7.90 MLd	40	BWTX/141
23 Johanna Foods	Johanna Foods	Food & Bev	Upgrade	Under Constrn	USA	G	1.51 MLd	4500	BWTX/561
24 RPM	H ₂ Flow	Plastics Recycling	New	Under Constrn	Canada	A	0.20 MLd	737	BWTX/9
25 Wickford Village	Ricci Drain-Laying Co., Inc.	Municipal Package Plant	New	2013	USA	D	0.10 MLd	12	BWTX/9
26 Garcia, Blummenau	Memphis Empreendimentos	Municipal	New	2013	Brazil	A	11.35 MLd	84	BWTX/120
27 Camp Neosa	Stephen Buckley	Municipal Package Plant	New	2013	USA	A	0.10 MLd	250	BWTX
28 Vitasoy	Vitasoy	Food & Bev	Upgrade	Under Constrn	USA	G	0.57 MLd	7,000	BWT-S
29 Givaudan Fragrance	Process Equipment Sales	Pharmaceutical New	New	New/Design	USA	G	0.15 MLd	5,000	BWTX
30 Waste Management	Aqua Tec	Leachate	Upgrade	2013	USA	A	0.04 MLd	500	BWTX
31 Vigor - Lima Duarte (MG)	Memphis	Food & Bev Dairy	Upgrade	2013-2014	Brazil	A	0.50 MLd	2,500	BWTX/108
32 Vigor - Santa Rita de Ibitipoca (MG)	Memphis	Food & Bev Dairy	Upgrade	2013-2014	Brazil	A	0.25 MLd	2,500	BWTX/54
33 Norsk Spesialolje	NSO AS	Industrial	New	2013	Norway	G	0.19 MLd	120	BWT X
34 Saulekilen RA	Sweco AS	Municipal	Upgrade	2014	Norway	A	25.44 MLd	200	BWT15

Type of technology

A	CMFF®
B	CMFF®(MBBR)
C	CMFF®(MBBR)/Chemical Precip
D	CFAS®
E	CFAS®/ Flotation
F	CFAS®/ Flotation (turnkey)
G	CFIC®

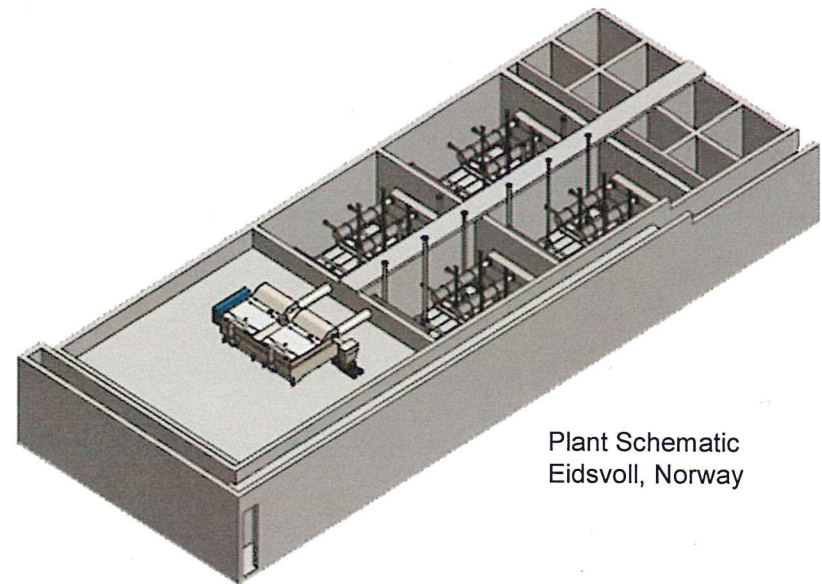
West Side Treatment Example

- CRD specification
 - ◆ 2x dry weather flow
 - ◆ Secondary treatment
 - ◆ Discharge to sea
- Biowater/Pivotal approach
 - ◆ 4x dry weather flow
 - ◆ Tertiary disinfected
 - ◆ Reuse water or recharge creeks
 - ◆ 25m x 50m footprint
- Differences
 - ◆ 2km outfall
 - ◆ Near-waterfront or waterfront siting
 - ◆ Footprint, just-in-time expansion
 - ◆ Lower capital & operating cost, debt impacts

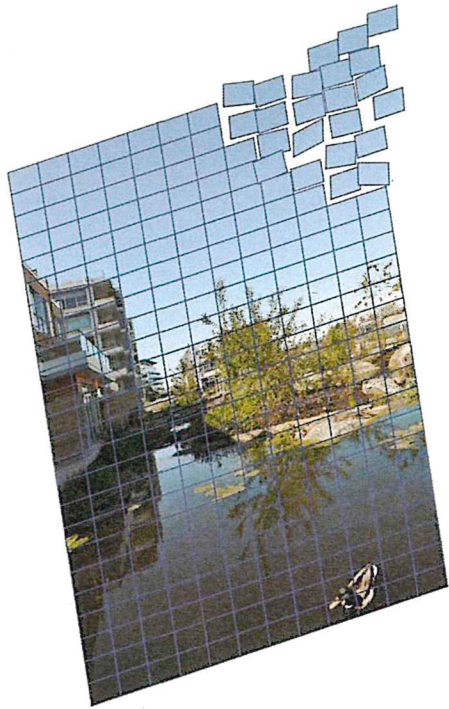


CFIC[®] System Benefits

- Enables distributed tertiary treatment
 - ◆ Low capital and operating costs
 - ◆ Highly scalable and compact
 - ◆ Modular design
- Avoids over-building large systems
 - ◆ Expand as/when/where needed
 - ◆ Minimizes taxpayer debt
- Dewateres sludge on-site
- Concentrates & manages hazardous & toxic compounds
- Reduce greenhouse gas emissions
- Maximizes resource recovery



Plant Schematic
Eidsvoll, Norway

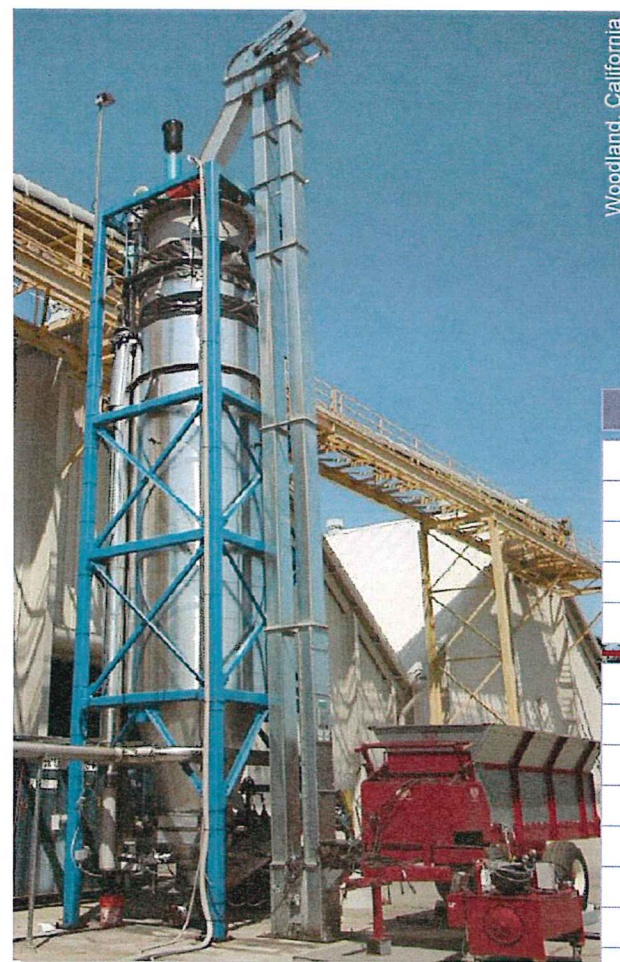


Pivotal IRM

Advanced Gasification

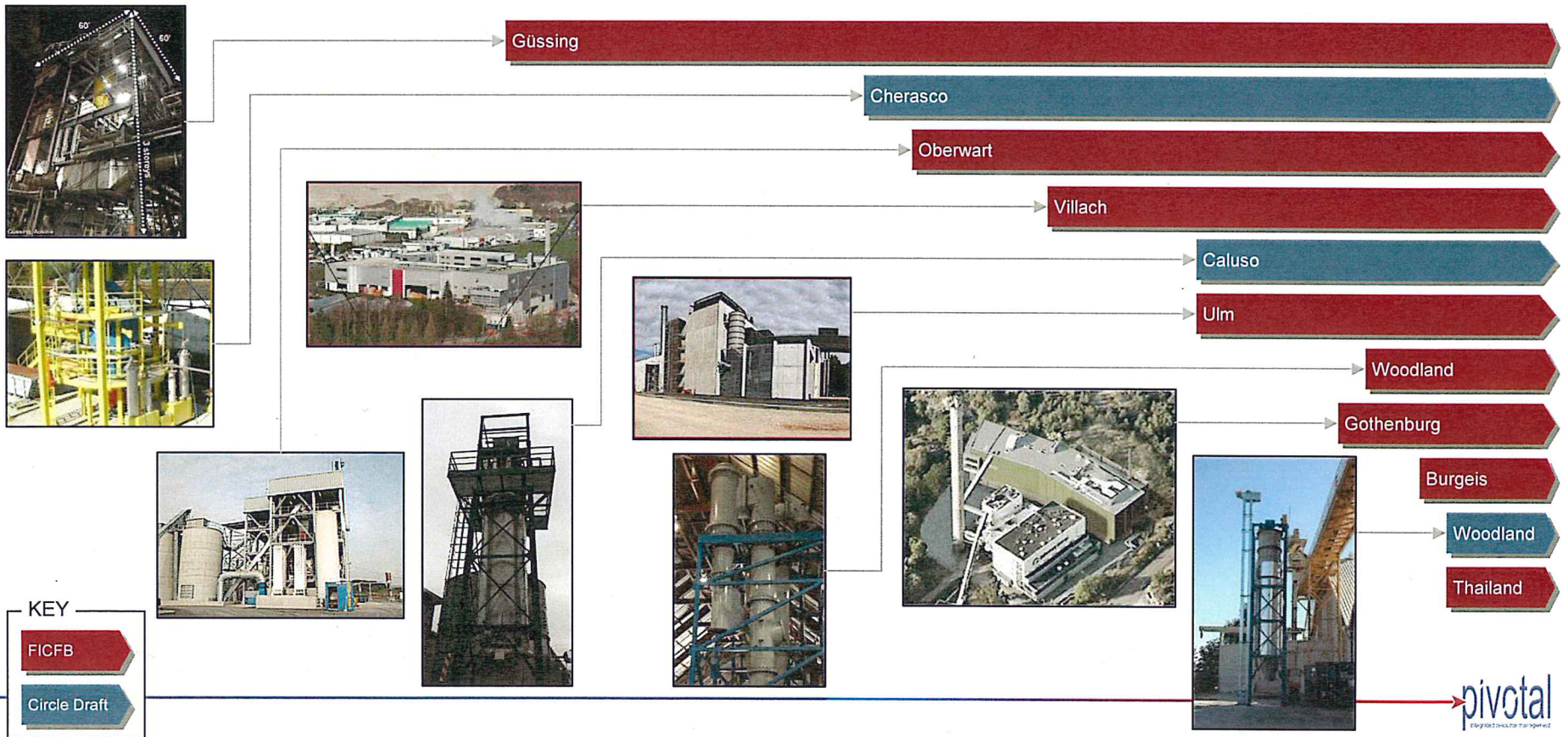
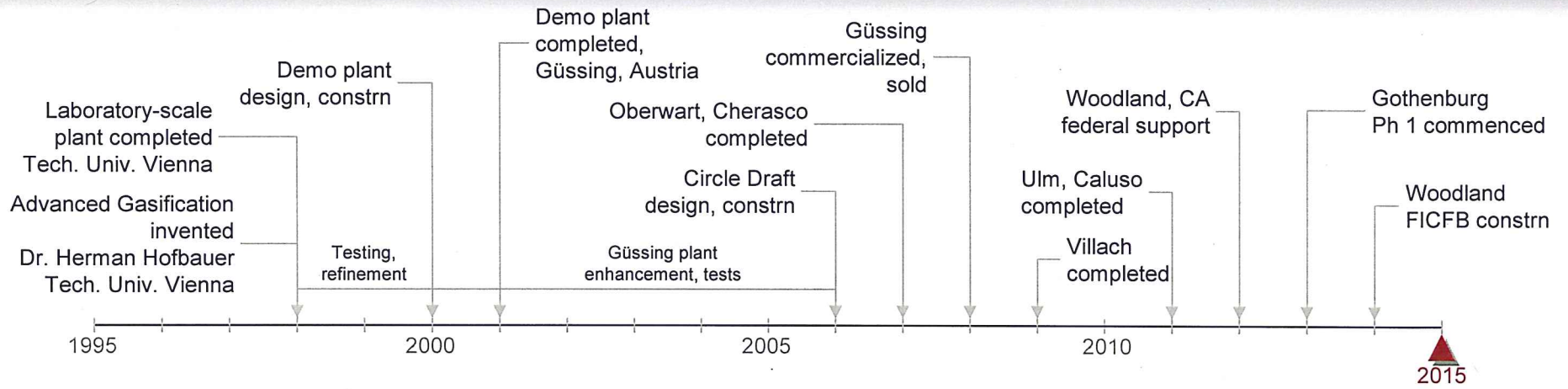
Technology

- Circle Draft Advanced Gasifier
 - ◆ Not incineration
 - ◆ Modified updraft gasification process
 - ◆ Developed since 2007
- Modular system
 - ◆ Single unit: 11 tonnes biomass/waste per day
 - Multi-unit systems for CRD
 - ◆ Feedstock: wood, MSW/RDF, sludge, etc
 - ◆ ≈12 months delivery
- Output
 - ◆ Energy
 - Heating, cooling
 - 500 kW electricity and 790 kW heat (ea.)
 - ◆ Biochar and ash
 - ◆ Distilled water
 - ◆ Emissions: ≈natural gas boiler



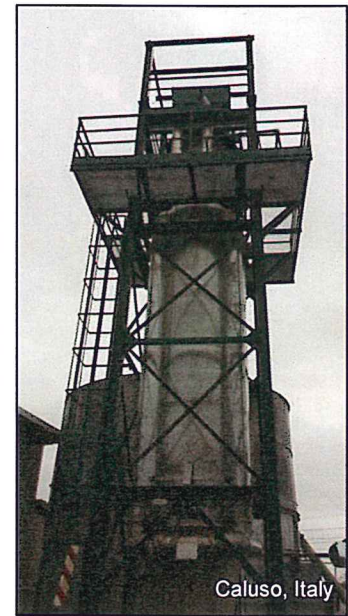
Woodland, California

Composition	
H ₂	20-33%
CO	16-47%
CH ₄	~2-4%
CO ₂	~0-14%
H ₂ :CO	1:1
C ₂ H ₄	2-3%
C ₂ H ₆	~0.5%
C ₂ H ₂	~0.4%
O ₂	< 0.1%
N ₂	1-3%
C ₆ H ₆	~8g/m ³
C ₇ H ₈	~0.5g/m ³
C ₁₀ H ₈	~2g/m ³
TARS	~20mg/m ³



Sludge Options – Circle Draft Advanced Gasifier

- Three operating plants
 - ◆ Cherasco & Caluso, Italy – 2007, 2011
 - ◆ Woodland, CA – Under commissioning
 - ◆ **50/50 mix of sludge/biomass**
- Benefits
 - ◆ Extremely small, nearly silent, safe
 - ◆ Low Capital and Operating costs
 - ◆ Generate green energy
 - Heating, cooling & power
 - Clean as natural gas
 - Complies with Clean Energy Act
 - ◆ Increases recycling
 - ◆ Address ≈60% of Hartland's volume



Comparison of Gasification Technologies

Criteria	FIXED BED GASIFIERS				ROTARY KILN	FLUIDIZED BED GASIFIERS	
	Grate	Updraft	Downdraft	Circle Draft Advanced Gasifier	Inclined	Stationary	FICFB
Feedstock variability	limited	limited	limited	multifuel	moderate	moderate	multifuel
Feedstock processing	low	moderate	moderate	high	low	high	high
Gasification agent	air	air	air	air/steam	air/steam	air/steam	steam
Robustness	moderate	moderate	moderate	high	moderate	moderately high	high
Gasifier Temperature	600 °C	550 °C	1000 °C	1050 °C	500 °C	650 °C	850 °C
Energy recovery efficiency	80%	80%	70%	<75%	70%	80%	89%
Tars (mg/m ³)	1,000	1,000	1,000	<20	500	50	20
Flyash (Kg/Tonne)	>50	>50	50	N/A	>50	25	8
Pollutant formation	high	high	moderate	low	high	moderate	low
Residual grate ash & biochar	5-20 %	5-20 %	5-20 %	15%	5-20 %	5-10 %	0%
Product gas							
Hydrogen	15	20	20	21	25	N/A	40
Carbon monoxide	10	10	10	30	20	N/A	22
Carbon dioxide	20	20	20	26	25	N/A	20
Methane	4	4	4	8	5	N/A	10
Other Hydrocarbons	3	0	0	5	3	N/A	5
Nitrogen	48	46	46	10	22	N/A	3
Calorific value (MJ/kg)	4	6	6	10	6	N/A	13

Generation Comparison

Anaerobic Digestion

263kw elec

+190%

Advanced Gasification

500kw elec

790kw thermal

"The calculations suggest that the ultra-high-temperature gasification (UHTG) system can achieve a net electrical energy output of about 15.40 MJ/kg (dry biosolids), whereas the AD system can achieve values between 8.45 MJ/kg (dry biosolids)."

ELECTRICAL ENERGY PRODUCTION FROM BIOSOLIDS: A COMPARATIVE STUDY BETWEEN ANAEROBIC DIGESTION AND GASIFICATION

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SUMMARY: Biosolids management is one of the most expensive and difficult processes in sanitation engineering. Anaerobic digestion is often employed for the stabilization of biomass and for energy production, as approximately 50% of the carbon entering the anaerobic digester is recovered as methane (CH₄). Gasification has been used recently for the thermal reformation of biosolids to synthesis gas (syngas), which primarily consists of carbon monoxide (CO) and hydrogen (H₂). In the present work has been calculated the net electrical energy production from biosolids, for a typical activated sludge wastewater treatment plant, with inlet flowrate of 75,708 m³/d (equal to 20 Mgd). The calculations suggest that the UHTG system can achieve a net electrical energy output of about 15.40 MJ/kg (dry biosolids), while the AD system can achieve values between 8.45 MJ/kg (dry biosolids). The latter yields 190% more electrical energy than the AD process. The net electrical energy output for UHTG, versus 9.9 kW for AD, for a typical activated sludge wastewater treatment plant, the UHTG process yields approximately 190% the

1 INTRODUCTION

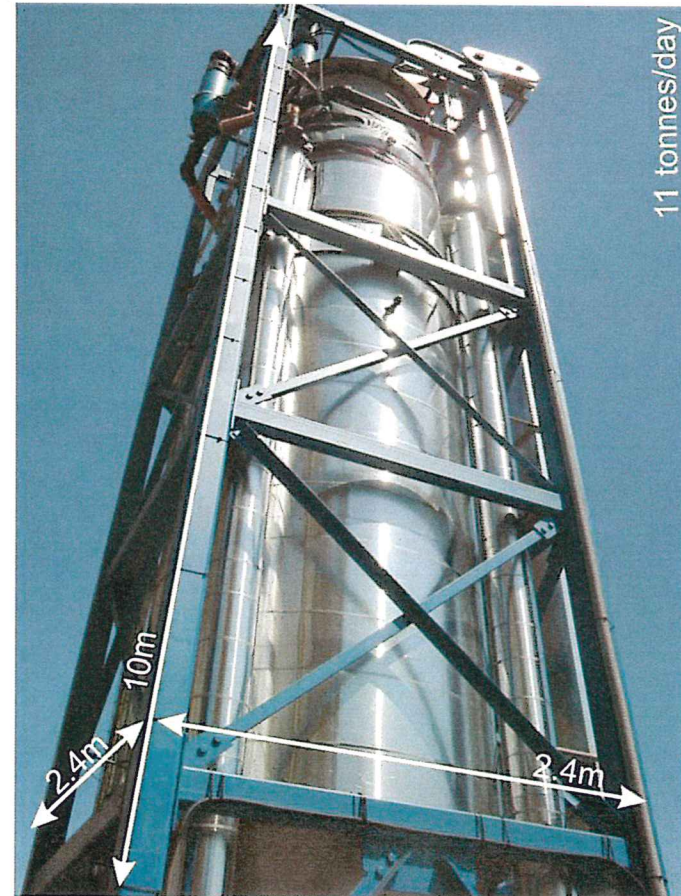
1.1 Background

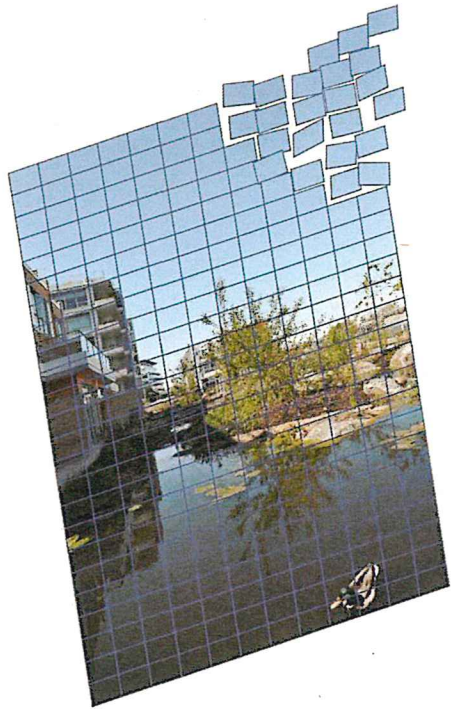
Biosolids (the semisolid by-product of wastewater treatment, consisting primarily of organics) management is one of the most expensive and difficult processes in sanitation engineering. Biosolids are considered as a nuisance because of their high organic content. Typical biosolids management processes include anaerobic digestion (AD), incineration, drying, and the chemical or biochemical stabilization (e.g., composting) (Tchobanoglous et al., 2003). Anaerobic digestion is the most prevalent process for biosolids management. The typical AD process is shown in Figure 1. AD is a biological process that involves the breakdown of organic matter into methane and carbon dioxide through the processes of hydrolysis and methanogenesis, with the latter being the rate-limiting step. The process is sensitive to various factors, such as time, hydraulic retention time, temperature, pH, and the presence of toxic substances (e.g., ammonia, heavy metals), and nutrient levels. During AD, a large fraction of the organics are converted into methane and carbon dioxide, while the remaining solids are sent to the residue. The produced biogas is often used to produce heat, or combined heat and electrical power (CHP). The heat is used to maintain the temperature inside the anaerobic digester within the optimal range. The primary reason for AD digestion is the stabilization of

CRETE2012
3RD INTERNATIONAL CONFERENCE ON INDUSTRIAL AND HAZARDOUS WASTE MANAGEMENT

Advanced Gasification Benefits

- Highly scalable, compact & modular, safe and odourless
- More efficient & fraction of the cost of anaerobic digestion
- Destroys harmful materials from entering water and/or land
- Maximizes resource recovery and revenues, improves recycling, maximizes diversion
- Reduces greenhouse gas emissions
- Stimulates economic development
 - ◆ Local jobs, R&D, manufacturing
 - ◆ Training and education
 - ◆ Tourism
- Flagship for green energy/sustainability





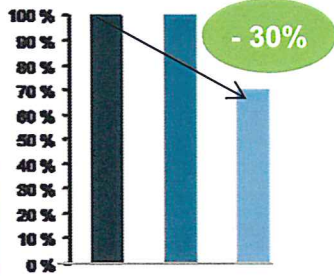
Putting It All Together

Why Integration Pays

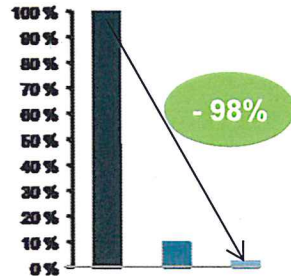
Alternative Approach

Tertiary Treatment

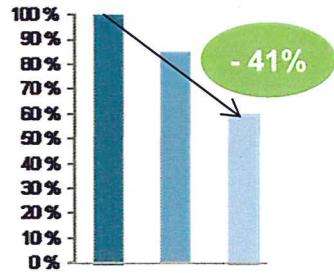
Energy consumption



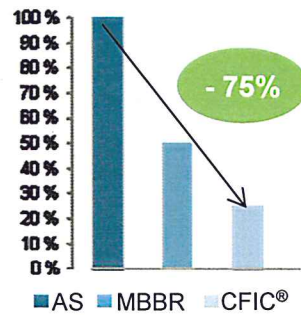
Solids in effluent



CAPEX

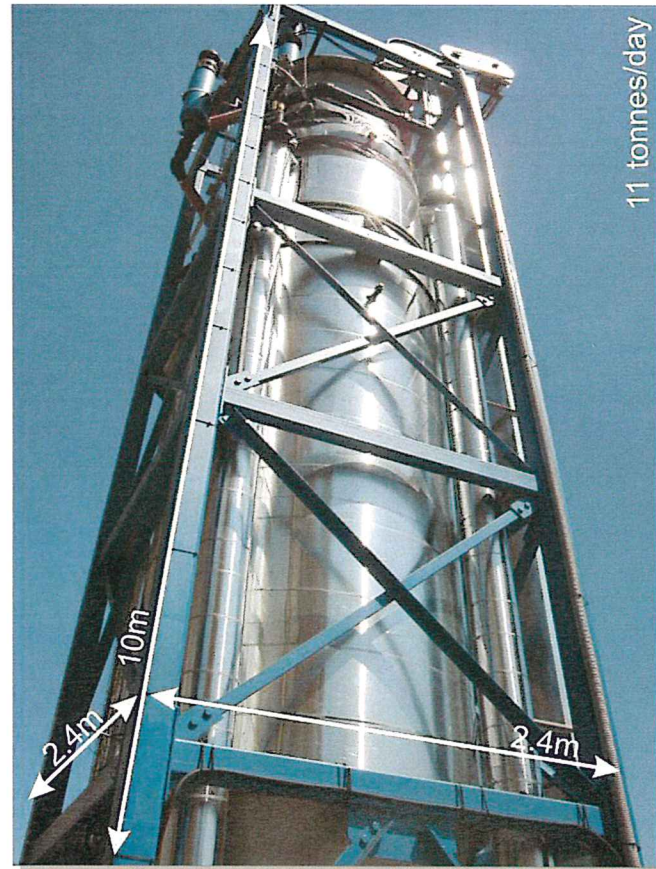


Space required



■ AS ■ MBBR ■ CFIC®

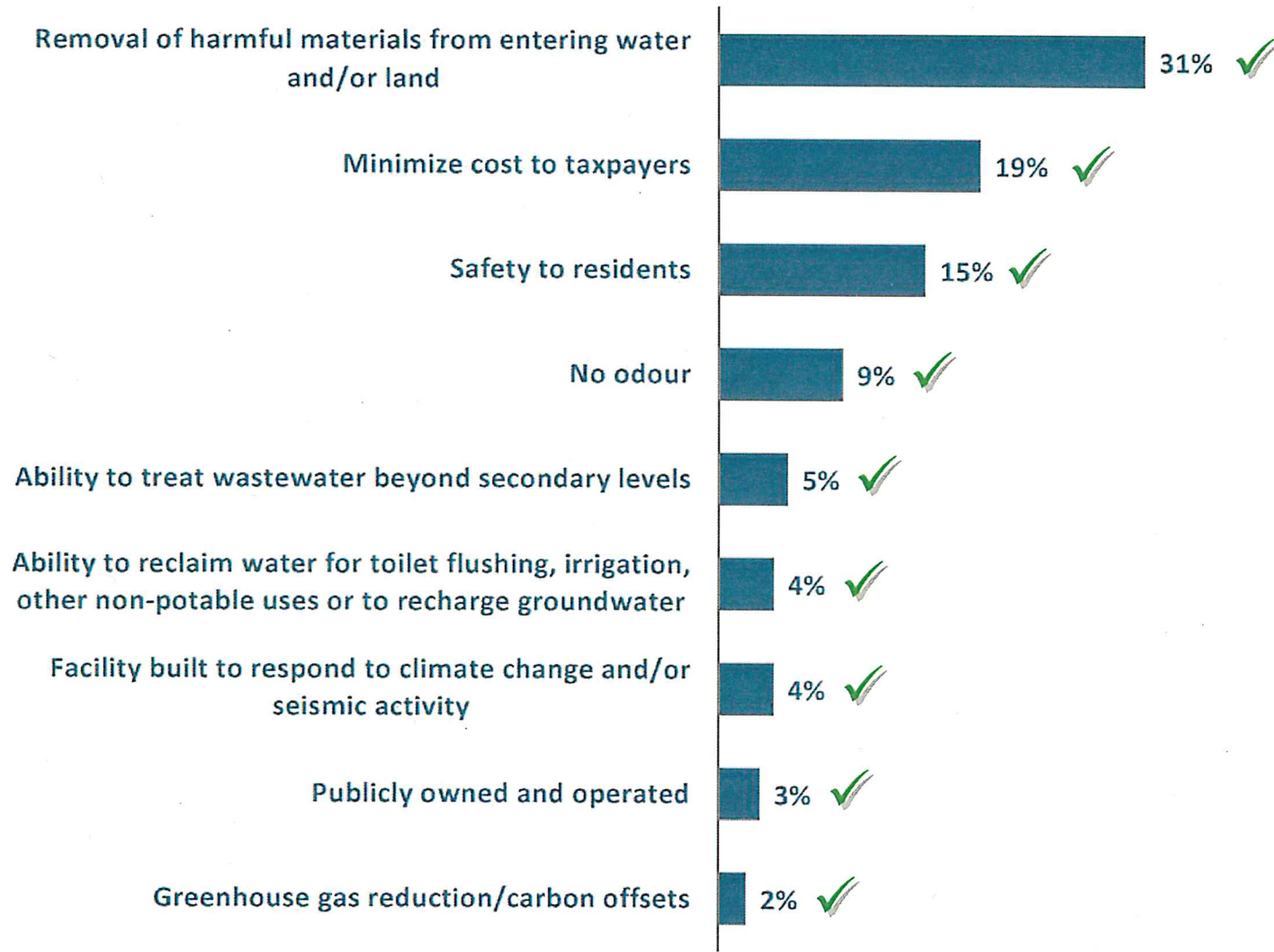
Advanced Gasification



Alignment with Community Objectives

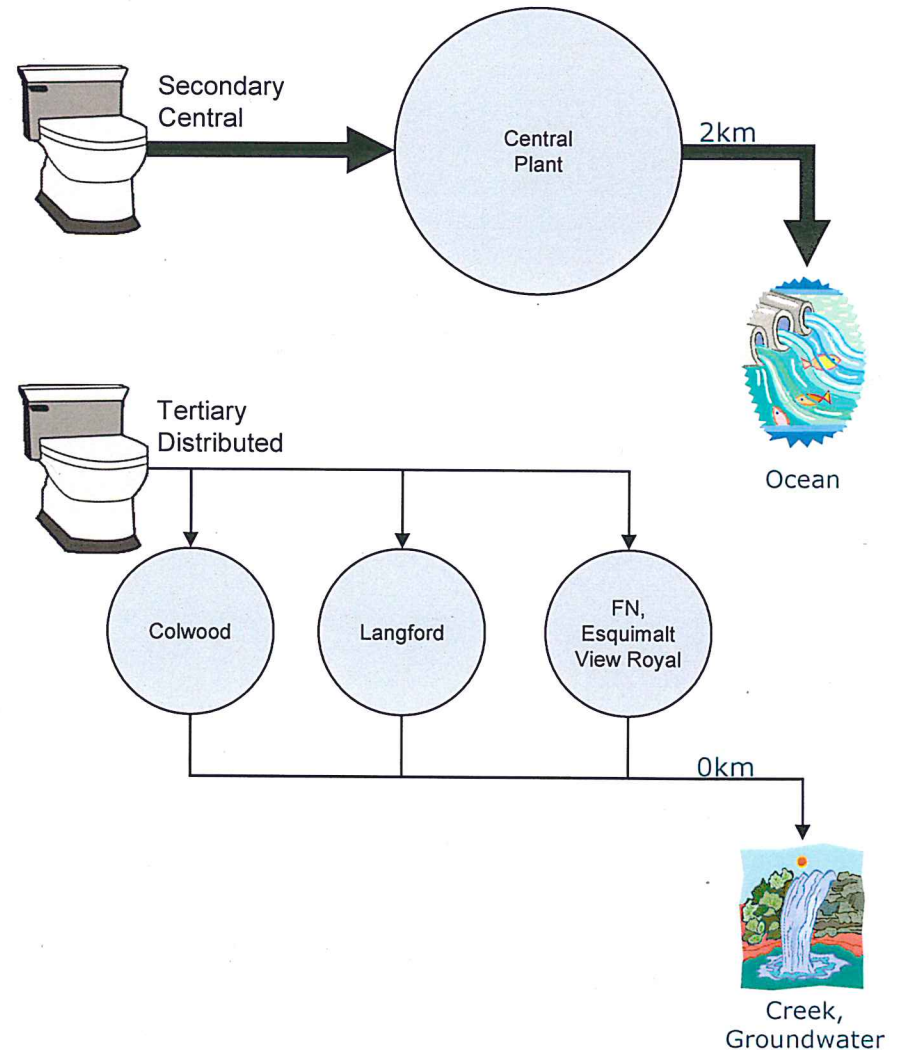


Most Important Criteria



Minimizing Impact, Maximizing Advantages

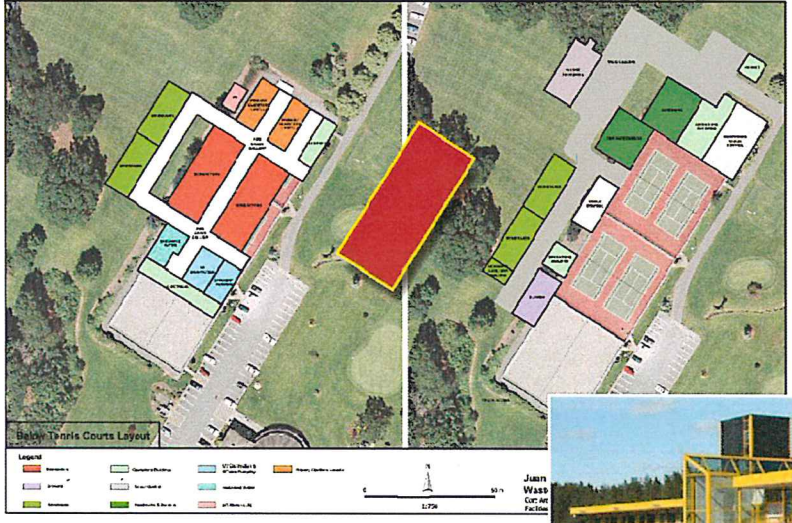
- Suitable for both distributed & centralized
- Distributed has advantages
 - ◆ Cost advantages
 - Avoids new pipes
 - Reduced or similar capital & operating cost
 - Reduced taxpayer charges and debt load
 - Considerably lower developer cost
 - ◆ Resilience & risk management
 - Reuse/recycling of heat & water maximized
 - Localized expansion as/when/where needed
 - ◆ But: extra public process
- Treatment site comparison
 - ◆ 036-DP west side : 38,202 m²
 - ◆ Pivotal/Biowater : ≈2,000 m² (<5%)
 - ◆ Minimal site impact – locate in spare land



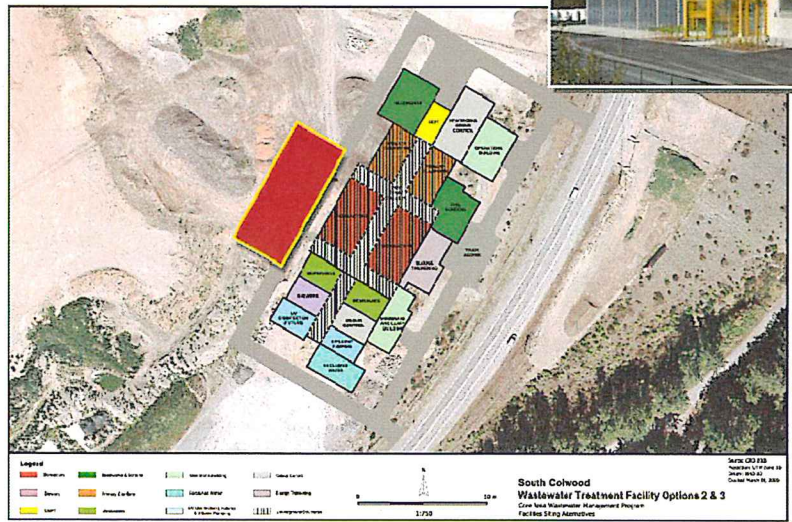
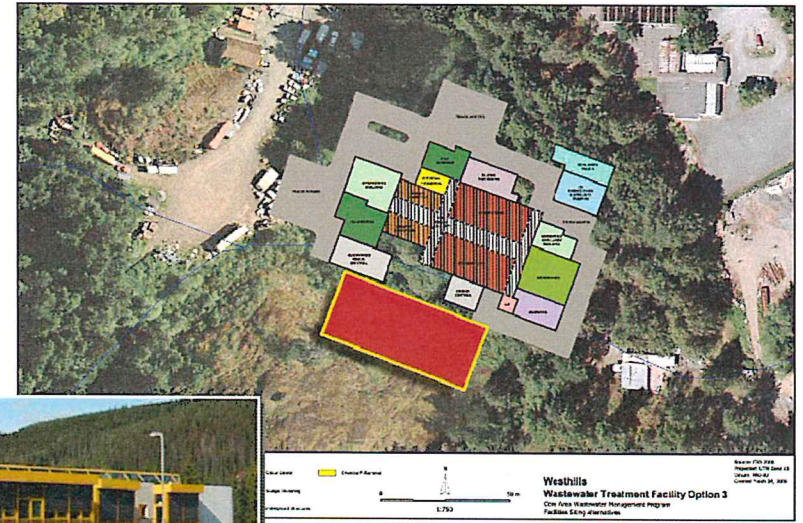
036-DP : Four West Side Sites



Juan de Fuca



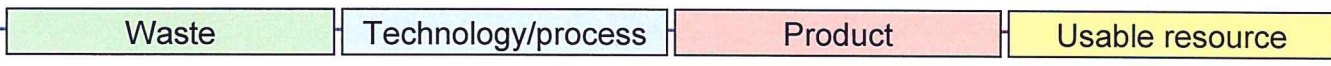
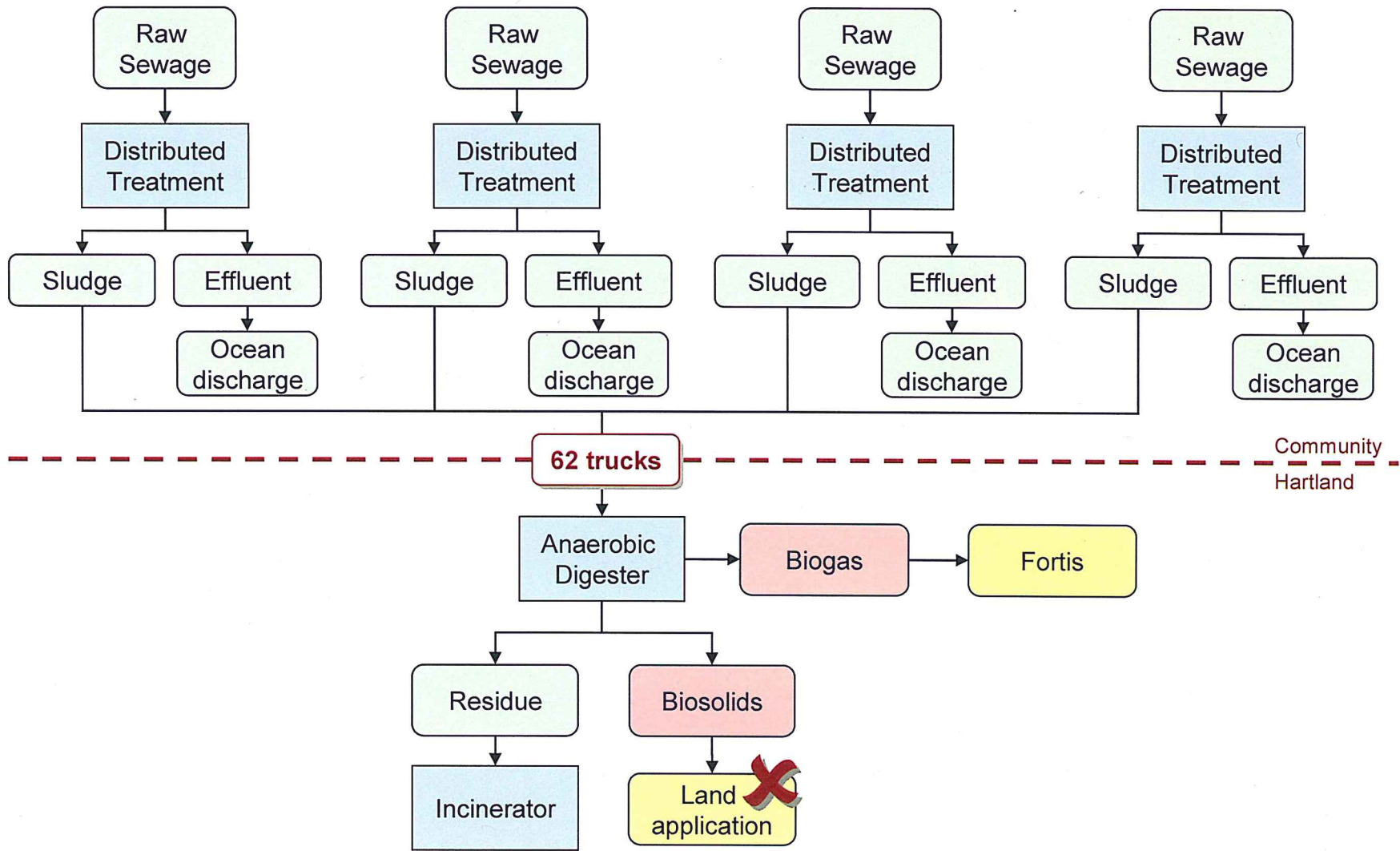
Westhills



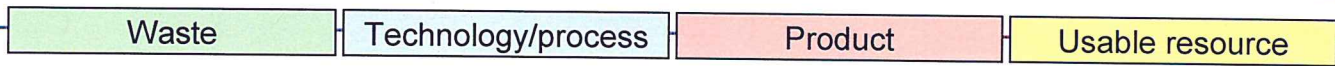
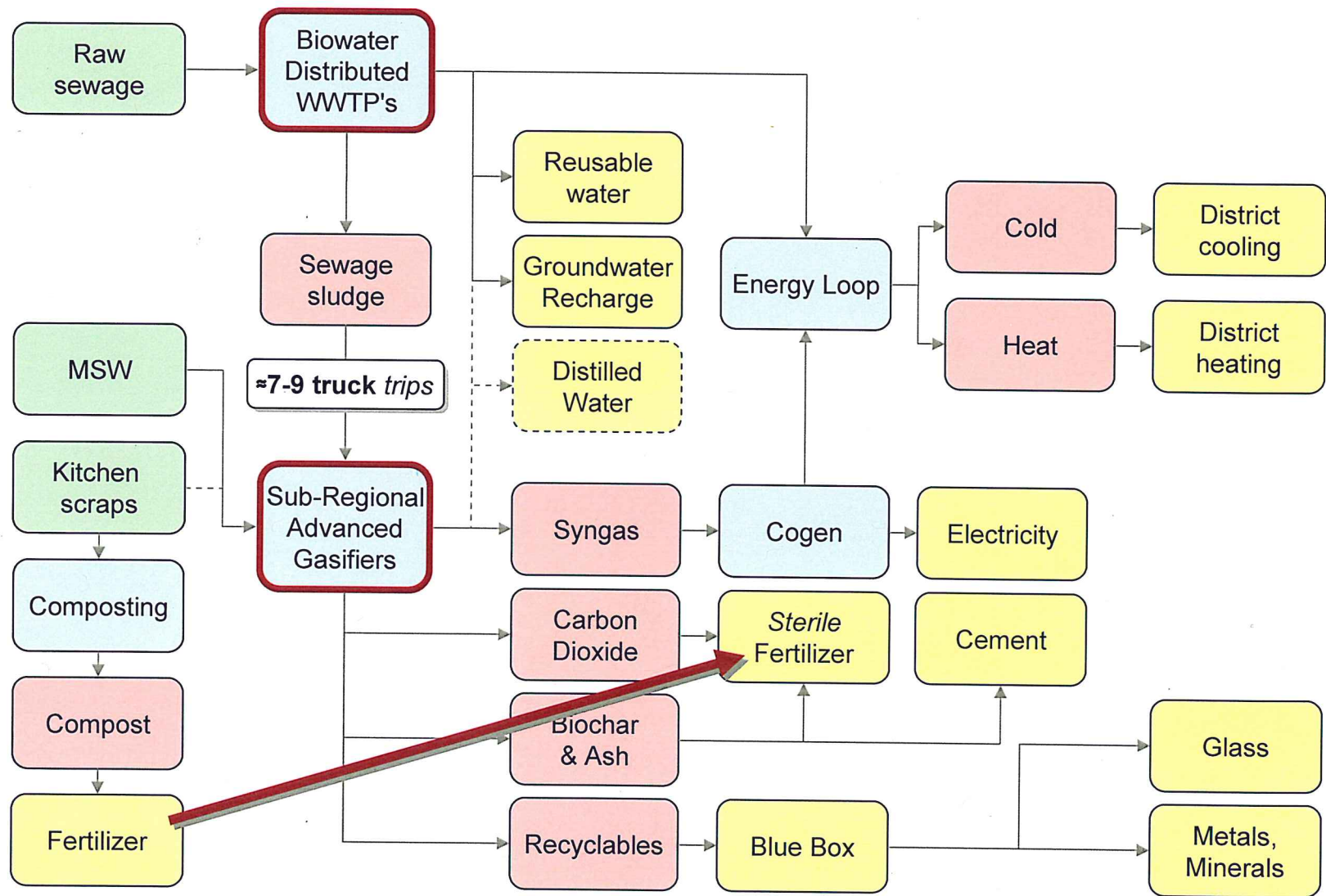
Royal Bay

Florence Lake

Trucking Sludge to Gasifier

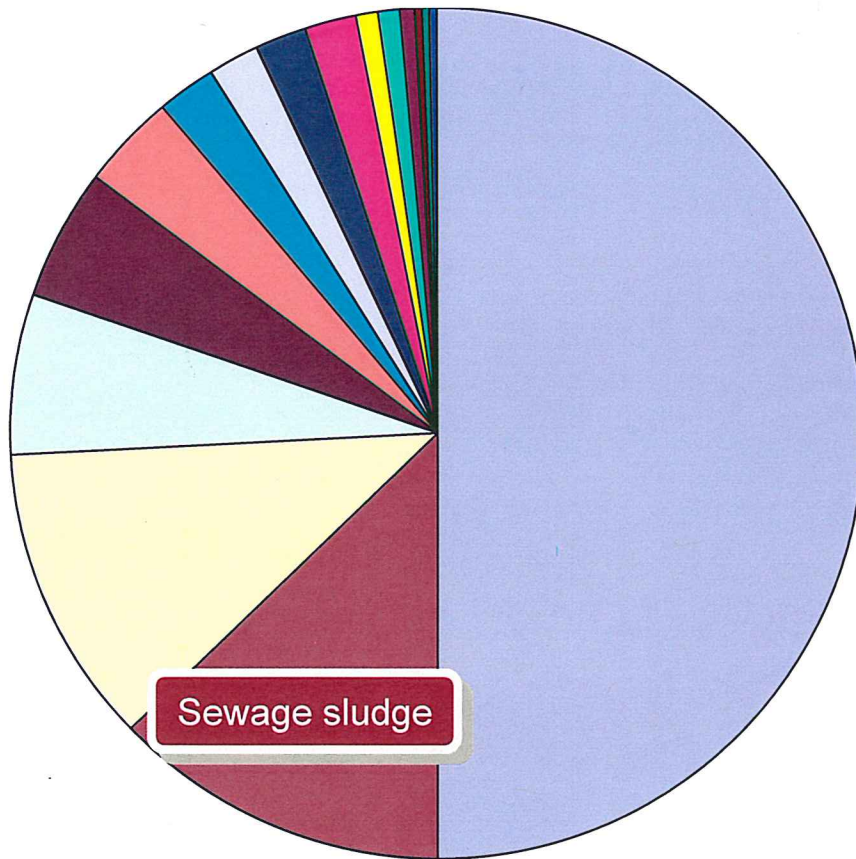


Trucking Sludge to Gasifier

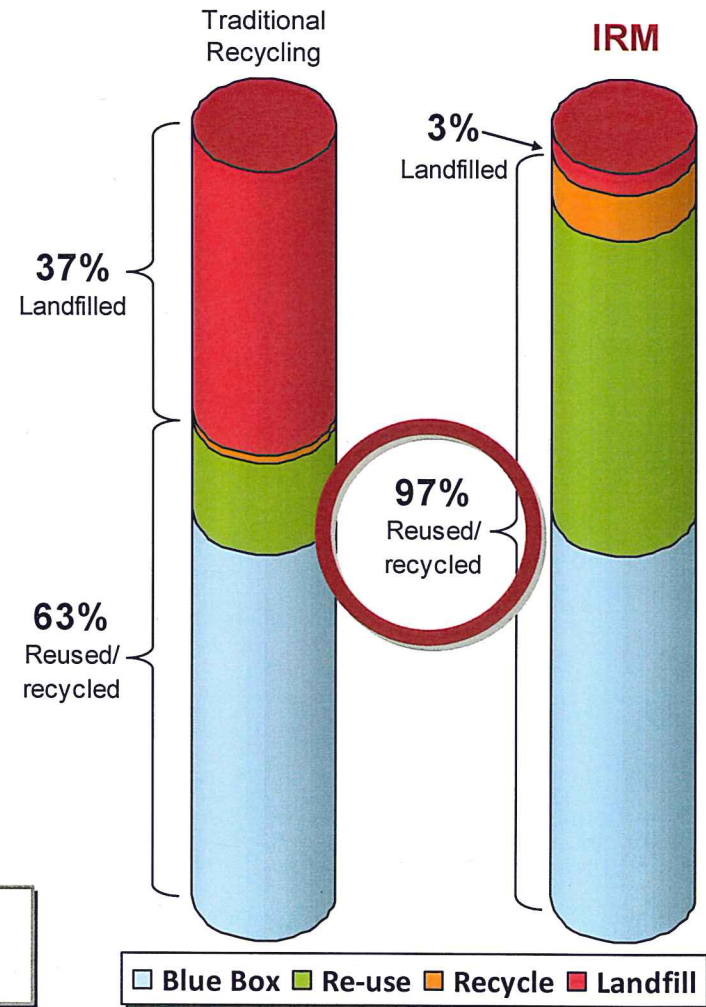


Incidental Benefit : 97% Maximum Diversion

Hartland Landfill Composition Study, 2011



- | | | | |
|--------------------|------------------------|-----------------------------|----------------------|
| Blue Box program | Sewage sludge | Organic Waste | Paper and Paperboard |
| Plastics | Wood and Wood Products | Construction and Demolition | Textiles |
| Composite Products | Other | Ferrous Metal | Glass |
| Electronics | Hazardous Waste | Rubber | Non-Ferrous Metal |



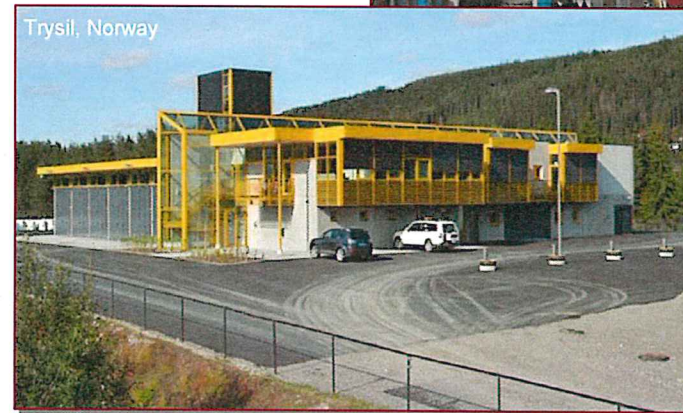
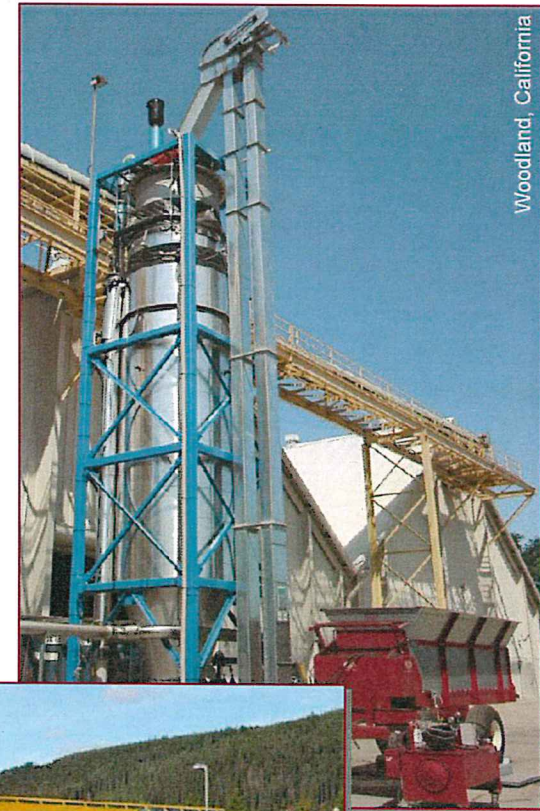
Summary

CRD data	Total	East side	West side
<i>Total projected sewage volume</i>	108 ML/day	83 ML/day	25 ML/day
<i>Total average daily sludge volume</i>	29 TPD	22 TPD	7 TPD
Pivotal/Biowater			
Potential recycled water	39,026 ML/yr	29,968 ML/yr	9,058 ML/yr
Potential distilled water	27 ML/yr	21 ML/yr	6 ML/yr
Potential electrical generation	43,800 mwh/yr	33,634 mwh/yr	10,166 mwh/yr
Potential thermal generation	69,204 mwh/yr	53,142 mwh/yr	16,062 mwh/yr
Potential char production	3,592 t/yr	2,759 t/yr	834 t/yr
Potential GHG CO ₂ e reduction	265,841 t/yr	204,141 t/yr	61,700 t/yr

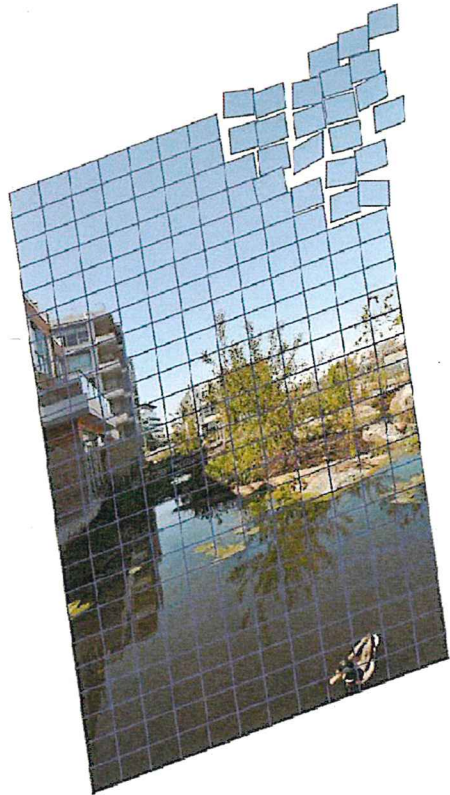
	Total Capital	LCC
CRD Plan	\$784m	\$3.2bn
Pivotal/Biowater	≈ \$250m	???

Summary & Conclusions

- Technologies are proven & stable
- Small plant size empowers & enables options
- "Future proof"
 - ◆ Economic modern technologies that exceed all environmental and financial standards
 - ◆ Scalable, J-I-T solutions
 - ◆ Simple to expand; reduces both current taxpayer and developers' costs
- Driven by a combined financial & environmental business case
 - ◆ *Focus: taxpayer & environmental value*



Questions



Thank you

